

CALCULATING FLUID FRICTION WITH FORMULAS

HEAD

FRICTION LOSS (DARCY-WEISBACH)

$$\frac{HF}{L} \left(\frac{\text{ft of fluid}}{100 \text{ ft of pipe}} \right) = \frac{1200 \times f}{D (\text{in})} \times \frac{(V (\text{ft/s}))^2}{2 \times 2 \left(\frac{\text{ft}^2}{\text{s}^2} \right)}$$

VELOCITY

$$V (\text{ft/s}) = 0.4085 \times Q (\text{gpm})$$

REYNOLDS NUMBER $\frac{V (\text{ft/s}) \times D (\text{in})}{\nu}$

$$Re = 7745.8 \times \frac{V (\text{ft/s}) \times D (\text{in})}{\nu (\text{cst})}$$

COLEBROOK EQUATION - FRICTION FACTOR f

$$\frac{1}{\sqrt{f}} = -2 \log_{10} \left[\frac{E (\text{ft})}{3.7 \times D (\text{ft})} + \frac{2.51}{Re \times \sqrt{f}} \right]$$

LAMINAR FLOW EQUATION - FRICTION FACTOR

$$f = \frac{64}{Re}$$

HF: FRICTION LOSS

L: PIPE LENGTH

f: FRICTION PARAMETER

D: INTERNAL PIPE DIA.

V = VELOCITY

Q = GRAVITATIONAL ACC.

32.17 ft/s²

Re = REYNOLDS NUMBER

ν = ABSOLUTE VISCOSITY

E = PIPE ROUGHNESS

DARCY-WEISBACH

FRICTION FACTOR f

$$f = \frac{H_f}{L}$$

HEAD LOSS

$$\left(\frac{L}{D}\right) \times \frac{V^2}{2g}$$

VELOCITY HEAD

2 CHARACTERISTIC LENGTHS

$$\frac{H_f}{L} \left(\frac{ft \text{ of head}}{100 \text{ ft pipe}} \right) = 1200 \times f \times \frac{(V(ft/s))^2}{2 \times 32}$$

EXAMPLE: $f = 0.03$ $E = 0.00015 \text{ ft}$ $D = 0.464 \text{ in} \frac{E}{D} = 0.00015 \times 12 = \frac{0.0038}{0.464}$

FROM MOODY DIAGRAM $g = 32.17 \text{ ft/s}^2$

$$V = \frac{0.4085 \times 6}{0.464^2} = 11.38$$

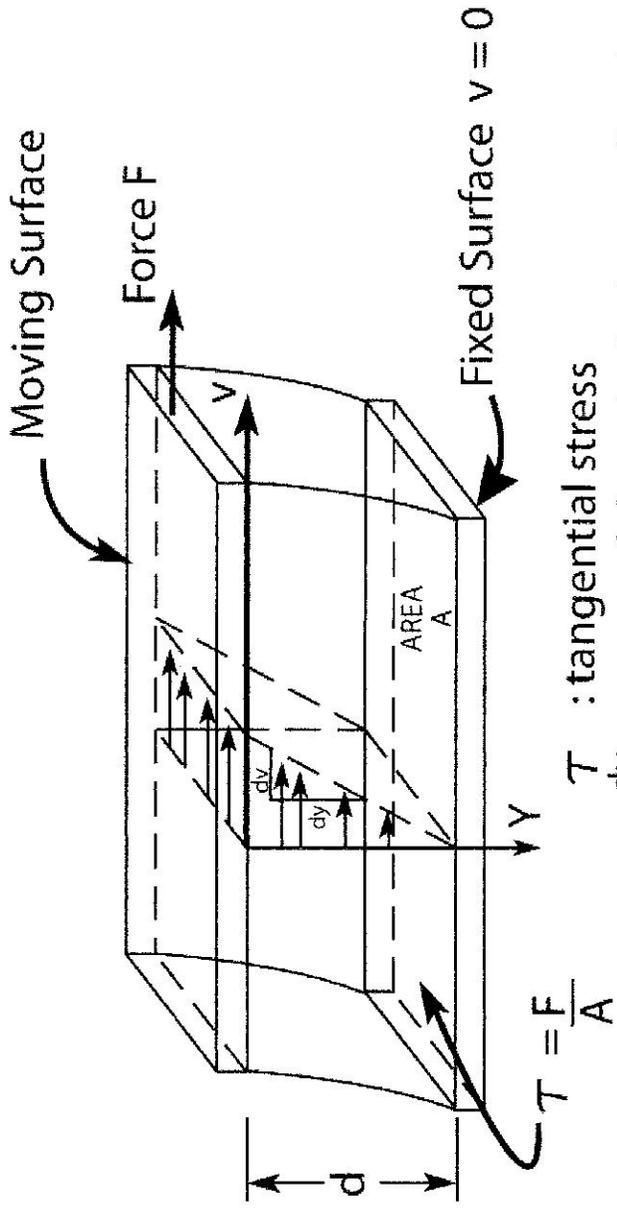
$$\frac{H_f}{L} = \frac{1200 \times 0.03}{0.464} \times \frac{11.38^2}{2 \times 32.17} = 158$$

REYNOLDS NUMBER

$$Re = 7745.8 \times \frac{V(\text{ft/s}) \times D(\text{in})}{\nu \text{ (cst)}}$$

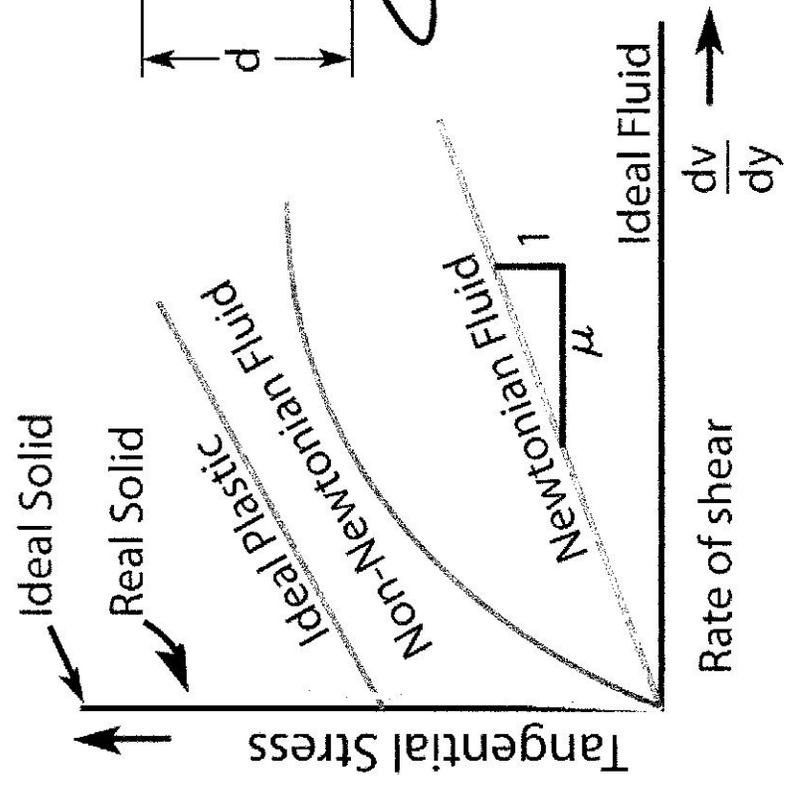
EXAMPLE: $V = 11.38$ $D = 0.464 \text{ in}$ $\nu = 1 \text{ cSt}$
FOR WATER

$$Re = 7745.8 \times \frac{11.38 \times 0.464}{1} = 4.09 \times 10^4$$



T : tangential stress
 $\frac{dv}{dy}$: rate of shear (velocity gradient)
 μ : viscosity

$$T = \frac{1}{\mu} \times \frac{dv}{dy}$$



FRICTION FACTOR f

COLEBROOK

$$\frac{1}{\sqrt{f}} = -2 \log_{10} \left(\frac{\epsilon (ft)}{3.7 \times D (ft)} + \frac{2.51}{Re \times \sqrt{f}} \right)$$

SWAMEE - JAIN

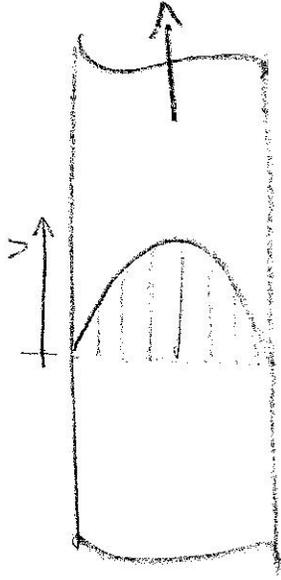
$$f = \frac{0.25}{\left(\log_{10} \left(\frac{\epsilon (ft)}{3.7 \times D (ft)} + \frac{5.74}{Re^{0.9}} \right) \right)^2}$$

EXAMPLE: $\epsilon/D = 0.0038$ $Re = 40900$

$$f = \frac{0.25}{\left(\log_{10} \left(\frac{0.0038}{3.7} + \frac{5.74}{40900^{0.9}} \right) \right)^2} = 0.031$$

LAMINAR FLOW

$$f = \frac{64}{Re}$$

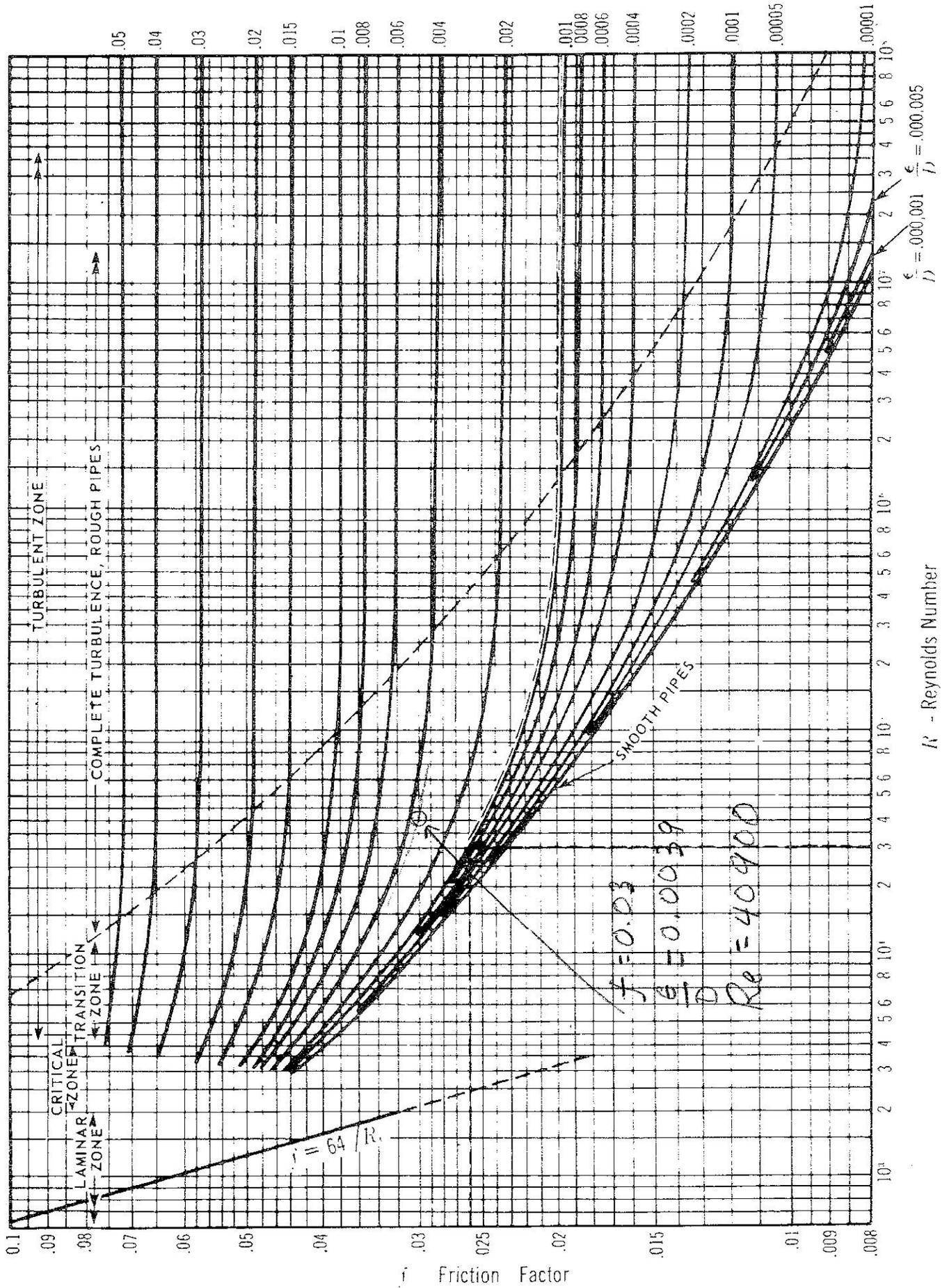


FLOW CORRESPONDS
TO AVERAGE VELOCITY

Friction Factors for Commercial Pipe

(for Darcy-Weisbach formula, page 3-3)

$$\text{Relative Roughness} = \frac{\epsilon}{D}$$



PIPE ROUGHNESS VALUES

Pipe absolute roughness values (RMS)		
Material	Absolute roughness (in x 10 ⁻³)	Absolute roughness (micron or m x 10 ⁻⁶)
Riveted steel ¹	36-360	915-9150
Concrete ¹	12-120	305-3050
Ductile iron ²	102	2591
Wood stave ¹	3.6-7.2	91-183
Galvanized iron ¹	6	152
Cast iron – asphalt dipped ¹	4.8	122
Cast iron uncoated ¹	10	254
Carbon steel or wrought iron ¹	1.8	45
Stainless steel ¹	1.8	45
Fiberglass ³	0.2	5
Drawn tubing – glass, brass, plastic ¹	0.06	1.5
Copper ²	0.06	1.5
Aluminium ²	0.06	1.5
PVC ²	0.06	1.5
Red brass ²	0.06	1.5

- Sources :
1. Cameron hydraulic data Book
 2. Engineered Software's PIPE-FLO software www.engineered-software.com
 3. Fiberglass Pipe Handbook, SPI Composites Institute

VISCOSITY

$$\nu \text{ (cst)} = \frac{\mu \text{ (cP)}}{SG}$$

- ν: KINEMATIC VISCOSITY
- μ: DYNAMIC VISCOSITY
- SG: SPECIFIC GRAVITY

$$SG = \frac{\rho_F}{\rho_W}$$

ρ_F: DENSITY OF FLUID

ρ_W: DENSITY OF WATER AT
STANDARD CONDITIONS
62.34 lbm/ft³

The Newton-Raphson iteration technique applied to the Colebrook equation

Since the value for f in the Colebrook equation cannot be explicitly extracted from the equation, a numerical method is required to find the solution. Like all numerical methods, we first assume a value for f , and then, in successive calculations, bring the original assumption closer to the true value. Depending on the technique used, this can be a long or slow process. The Newton-Raphson method has the advantage of converging very rapidly to a precise solution. Normally only two or three iterations are required.

The Colebrook equation is:

$$\frac{1}{\sqrt{f}} = -2 \log_{10} \left(\frac{\varepsilon}{3.7D} + \frac{2.51}{Re \sqrt{f}} \right)$$

The technique can be summarized as follows:

1. Re-write the Colebrook equation as:

$$F = \frac{1}{\sqrt{f}} + 2 \log_{10} \left(\frac{\varepsilon}{3.7D} + \frac{2.51}{Re \sqrt{f}} \right) = 0$$

2. Take the derivative of the function F with respect to f .

$$\frac{dF}{df} = -\frac{1}{2} f^{-3/2} \left(1 + \frac{2 \times 2.51}{\log_e 10 \times \left(\frac{\varepsilon}{3.7D} + \frac{2.51}{Re \sqrt{f}} \right) Re} \right)$$

3. Give a trial value to f . The function F will have a residue (a non-zero value). This residue (RES) will tend towards zero very rapidly if we use the derivative of F in the calculation of the residue.

$$f_n = f_{n-1} - RES \text{ with } RES = \frac{F}{\frac{dF}{df}}$$

For $n = 0$ assume a value for f_0 , calculate RES and then f_1 , repeat the process until RES is sufficiently small (for example $RES < 1 \times 10^{-6}$).

The Newton-Raphson iteration technique is a method that converges very rapidly to a solution. You need to provide a seed value for f_{n-1} to start the iteration and an acceptable error RES which you can make very small.